

A) Remarks:

According to the Office Action, claims 10-12 are rejected under 35 U.S.C. 102(b) and claims 13-21 are rejected under 35 U.S.C. 103(a) as being unpatentable over Japanese Publication 11-106770 (JP'770) alone or in view of Mandelik (3,771,261) and other references.

However, in view of the following remarks, reconsideration is respectfully requested. It is respectfully submitted that claims 10-21 should be allowed because claim 10 of this invention is quite different from JP'770.

The following is the comparison between this invention and JP'770.

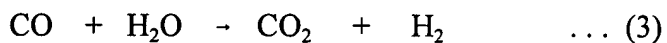
This invention relates to a method for producing safe town gas containing mainly methane by using dimethyl ether as feed stock. The gas produced by this invention has high calorie content and is safe because the gas hardly includes any carbon monoxide.

In the method for producing town gas according to claim 10, the steps comprise preparing dimethyl ether as feed stock, evaporating the dimethyl ether, and exothermically reforming the dimethyl ether in the presence of catalyst and steam to produce reformed gas containing mainly methane.

Such a method for producing town gas is carried out according to the following reaction equation (1), theoretically (Table 1):



In practice, hydrogen (H_2) and carbon monoxide (CO) are also produced besides methane (CH_4) and carbon dioxide (CO_2) with the reaction equation (1). Simultaneously, the following equations (2) - (4) proceed:

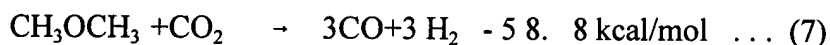
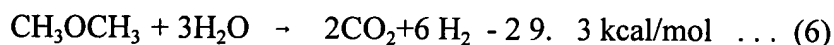
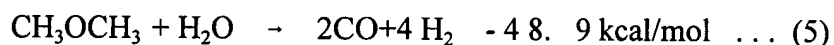


Accordingly, when dimethyl ether is reformed catalytically, the reformed gas contains H_2 , CO , CO_2 , H_2O , and mainly CH_4 . Compositions of the reforming gas vary with the reaction temperature, kinds of catalysts and so on. The compositions of the reformed gas, are about 50-70% CH_4 , 20-25% CO_2 , 10-30% H_2 and 0-3% CO , besides H_2O (Section [0016] of the original specification of this invention).

Examples 1-3 of this invention disclose concentrations of CH_4 and CO in the reaction product (except H_2O) at the outlet of the reforming reactor. The concentrations are 50% CH_4 and 1.9% CO in Example 1 (Table 2 [1k]), 74% CH_4 and 0.2% CO in Example 2 (Table 3 [2d]) and 72% CH_4 and 0.05% CO in Example 3 (Table 4 [3h]), respectively.

As described, high safety town gas can be produced by this invention because the concentration of CO is very low.

On the other hand, JP'770 relates to a method for producing synthetic gas or hydrogen gas by reforming dimethyl ether. The synthetic gas is the mixed gas of carbon monoxide (CO) and hydrogen (H₂). The reforming reaction of dimethyl ether is shown in the following equations (5) - (7) (Section [0012]).



The synthetic gas produced of these reaction equations (5) - (7) has low calorie content and includes a large quantity of CO that is harmful. Accordingly, this synthetic gas is improper to use as town gas in view of safety considerations.

For example, the concentration of CO in the reformed gas produced using catalyst examples 2, 5 and 27 of JP'770 are 39.6%, 34.6% and 52.2% respectively. These concentrations of CO are very high.

Further, the concentrations of hydrocarbon (such as methane) in the reformed gas produced using catalyst examples 2, 5 and 27 of JP'770 are 2.2%, 0.3% and 15.9%, respectively. These concentrations are much lower than the concentration of methane in the reformed gas produced by this invention.

As described, this invention and JP'770 are similar to each other in using dimethyl ether as feed stock. However, this invention and JP'770 are different from each other in the concentrations (yields) of CH_4 and CO in the produced gas. That is, this invention and JP'770 are quite different from each other with respect to the reforming process of dimethyl ether and the operation of steam, as the following explains:

1. With respect to the reforming process:

The reforming reaction of dimethyl ether in this invention is an exothermic reaction. On the other hand, the reforming reaction of JP'770 is an endothermic reaction.

The Examiner points out in the Office Action that the DME reforming reaction is an exothermic reaction and JP'770 discloses a reforming process with exothermic reactions. However, the Examiner is misunderstanding the reforming process of JP'770.

JP'770 definitely states that the reforming reaction of dimethyl ether according to this embodiment has a large heating value of an endothermic reaction (Section [0012]).

Further, above equations (5) - (7) show endothermic reactions. These reactions need much heat so that these reaction equations proceed toward the right side.

Furthermore, JP'770 discloses that the reforming reaction of dimethyl ether is carried out using waste heat at the temperature of 200-500 °C (claim 2 and Section [0011]). That is, the reforming reactions shown in the above equations (5)-(7) is carried out by supplying much heat from outside.

As described, the reforming reaction of JP'770 is obviously an endothermic reaction.

2. With respect to the operation of steam:

The reforming reaction of dimethyl ether concerning this invention is the reaction which does not consume water (H_2O). The reforming reaction shown in the above equation (1) is highly exothermic. Hence, when the temperature of the reaction system rises excessively, the reforming reaction will increase the amount of byproduced CO due to chemical equilibrium, so that deactivation of the catalyst will be promoted. In this invention, steam coexists for reforming reaction of dimethyl ether. The principal purpose of coexistence of steam is to suppress the temperature rise of the reaction system.

On the other hand, the reforming reaction of JP'770 is a reaction which consumes much water. Accordingly, this reaction system needs a large supply of water from outside. JP'770 discloses that the quantity of the steam to be supplied is 1 to 20 mol times the quantity of the dimethyl ether in order to obtain a high dimethyl ether conversion ratio (Section [0027]).

As described, this invention and JP'770 are different from each other also in the operation of steam.

3. With respect to the byproducts of the reforming process:

The Examiner also points out in the Office Action that JP'770 discloses methane as one of the reforming products with reaction temperature of 200-500 °C. However, it is the methane which is a higher undesirable byproduct. Concerning JP'770, methane is neither an object nor a main component. Referring to the data of catalyst examples of JP'770, the highest yield of hydrocarbon is 15.9% (example 27). In other examples, the yields are less than 10%.

On the other hand, this invention is a method for producing the gas containing mainly methane which is a kind of hydrocarbon. Concentration of methane in the reformed gas is 50-70% in this invention.

4. With respect to the reaction temperature:

The reforming temperatures are overlapped between this invention and JP'770. However, the DME reforming reaction of JP'770 is an endothermic reaction and the heat necessary for the reaction is obtained by heat exchange with exhaust gas (Section [0092]), Fig. 1).

On the other hand, the DME reforming reaction is an exothermic reaction in this invention. When dimethyl ether is supplied with a temperature of 300 °C at the inlet of the reforming reactor, the temperature of the exit gas of catalyst layer of the reactor rises to 545 °C (Table 2, Section [0047] of the original

specification of this invention). In this invention, the reforming temperature is controlled by the quantity of coexisting steam. Such operation of the steam is not disclosed in JP'770.

As above described, this invention and JP'770 are quite different from each other in these objects and functions, operations or effects. Accordingly, claims 10-12 of this invention should not be rejected based on JP'770 under 35 U.S.C. 102(b).

Further the claims 13-21 of this invention depend on claim 10 of this invention. Claim 10 is quite different from JP'770 as above mentioned. Accordingly, claims 13-21 also should not be rejected based on the combination of JP'770 and other prior art cited under 35 U.S.C. 103(a).

As the Examiner knows, references may only be combined, without the use of hindsight, for what they fairly teach to one of ordinary skill in the art. From the foregoing it can be readily observed that the combination of references cited by the Examiner teaches something quite different to one of ordinary skill in the art than what is claimed by Applicants. Accordingly the rejection of Applicants' claims under 35 U.S.C. 103(a) is considered to be inappropriate.

In view of the foregoing remarks, it is now believed that this application is in condition for allowance. Accordingly, favorable reconsideration with notice of allowance is requested.

Respectfully submitted,

CAROTHERS AND CAROTHERS



Floyd B. Carothers
Attorney for Ishigaki, et al.
Fort Pitt Commons, Suite 500
445 Fort Pitt Boulevard
Pittsburgh, PA 15219

FBC:jkc
Reg. No. 24,252
(412) 471-3575
(412) 281-2180
Pittpatent@aol.com

ET 793408893 US

I hereby certify that this correspondence is being deposited with
the United States Postal Service with sufficient postage as Express
Mail in an envelope addressed to: Commissioner for Patents,
P.O. Box 1450, Alexandria, VA 22313-1450, on April 7, 2005

CAROTHERS AND CAROTHERS

